

**Activated sludge:  
100 plus 1 years**  
New trends and perspectives

POLITECNICO DI MILANO  
UNIVERSITÀ DEGLI STUDI DI PALERMO

Palermo, May 11<sup>th</sup> 2015

➔ **Membrane bioreactors - MBRs**

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➔ **Membrane bioreactors - What are they? - 1** 2

### Membrane Bioreactors

**Activated sludge process**

Influent    Sludge recycle    Effluent

Aeration tank    Air    sludge recycle pump    Settling tank    Excess sludge

**Membrane bioreactor process**

Influent    Sludge recycle    Excess sludge

Aeration tank    Air    Pump    Membrane    Effluent

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**Membrane bioreactors - What are they? - 2** 3

Porosity (micrometers)	0.001	0.01	0.1	1.0
Porosity (Ångstrom)	10	100	1,000	10,000
Molecular Weight (Dalton)	200	20,000	100,000	500,000
Dimensions of different substances	Me <sup>++</sup> Salt solutions Sugars		Proteins Soot Emulsions Colloids	<b>Bacteria</b> Pigments, dyes
Separation processes	Reverse Osmosis Nanofiltr.	Ultrafiltration	Microfiltration	

Range of MBR

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**Membrane bioreactors - What are they? - 3** 4

FLAT-SHEET

HOLLOW FIBER

SPIRAL-WOUND


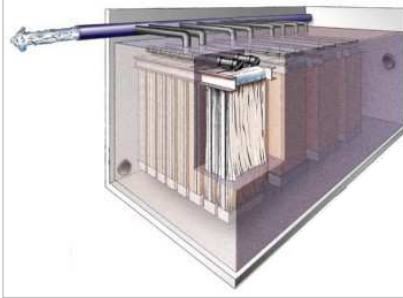
TUBULAR

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**Membrane bioreactors - What are they? - 4** 5

**EXTERNAL**

**INTERNAL**

Difference between the two:  
How filtration is operated and  
Cleaning methods

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**Membrane bioreactors - Milestones 1** 6

**1969 – 1985: Research**

**1969 – Lab scale**  
Smith, C. W., Di Gregorio, D., and Talcott, R. M. (1969). The use of ultrafiltration membrane for activated sludge separation. Proceedings of the 24th Annual Purdue Industrial Waste Conference, Purdue University, West Lafayette, Indiana, USA. 1300–1310.

**1971 – Dorr Oliver MBR shipboard systems**  
Bemberis I., et al. (1971) Membrane sewage treatment systems-potential for complete wastewater treatment, Pamer. Soc. Agric. Eng. Winter Mtg. 71-878, 1-28.

**1985 – Dorr Oliver concept of anaerobic side stream MBR systems**  
Li A., et al., 1985, Application of membrane anaerobic reactor system (MARS) for treatment of industrial wastewaters. Proc. 39<sup>th</sup> Ind. Waste Conf., Purdue University, Lafayette, Indiana, USA, May, 627-636

**The 90's: Prototypes**

**1989 – First hollow fiber (HF) UF MBRs**  
Yamamoto K, Hiasa H, Talat M, and Matsuo T (1989) Direct solid liquid separation using hollow fiber membranes in activated sludge aeration tank. Water Science and Technology 21: 43–54.

**1991 – First flat sheet (FS) UF MBRs**  
Ishida, H., Yamada, Y., Tsuboi, M., and Matsumura, S. (1993). Submerged membrane activated sludge process (KSMASP) — its application into activated sludge process with high concentration of MLSS. Proceedings of the 2nd International Conference on Advances in Water and Effluent Treatment

**1993 – Kubota (FP), Mitsubishi (SUR) and Zenon (ZW145-50): first commercial MBRs**

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## Membrane bioreactors - Milestones 2

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**From 2000: Commercial development**

- Microdyn-Nadir BioCel (FS, D)
- HuberVRM (FS, D)
- Toray (FS, J)
- MemStar (HF, PRC)
- Econity (HF, South Korea)
- Anaergia FiberPlate (HF, Canada)
- Puron (now Koch Membrane System - KMS)
- Zenon ZW-500d (HF, CN, now GE, USA)
- US Filter MemJet (HF, USA)

**From 2008: Optimization**

- Siemens Memcor MemPulse (now Evoqua HF, USA)
- Puron-KMS PVDF module (HF, USA)
- GE LEAP MBR (HF, USA)
- Kubota RW type 300, 200, 150 (FS, J)
- ...& others

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## Membrane bioreactors - Trend of technical papers

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*Papers with MBR + wastewater in title*

Year	Number of Papers
1990	0
1991	0
1992	0
1993	0
1994	0
1995	0
1996	0
1997	0
1998	0
1999	0
2000	0
2001	0
2002	0
2003	0
2004	0
2005	0
2006	0
2007	0
2008	0
2009	0
2010	0
2011	0
2012	0
2013	0
2014	0

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### Membrane bioreactors - Books and websites

Judd, 2011



Hai et al. 2013 (IWA)



Brepols, 2010 (IWA)



WEF Manual of Practice no. 36, 2012



<http://www.mbr-network.eu/mbr-projects/downloads-common.php>  
 [www.thembrsite.com](http://www.thembrsite.com)  
[www.onlinembr.info/](http://www.onlinembr.info/)

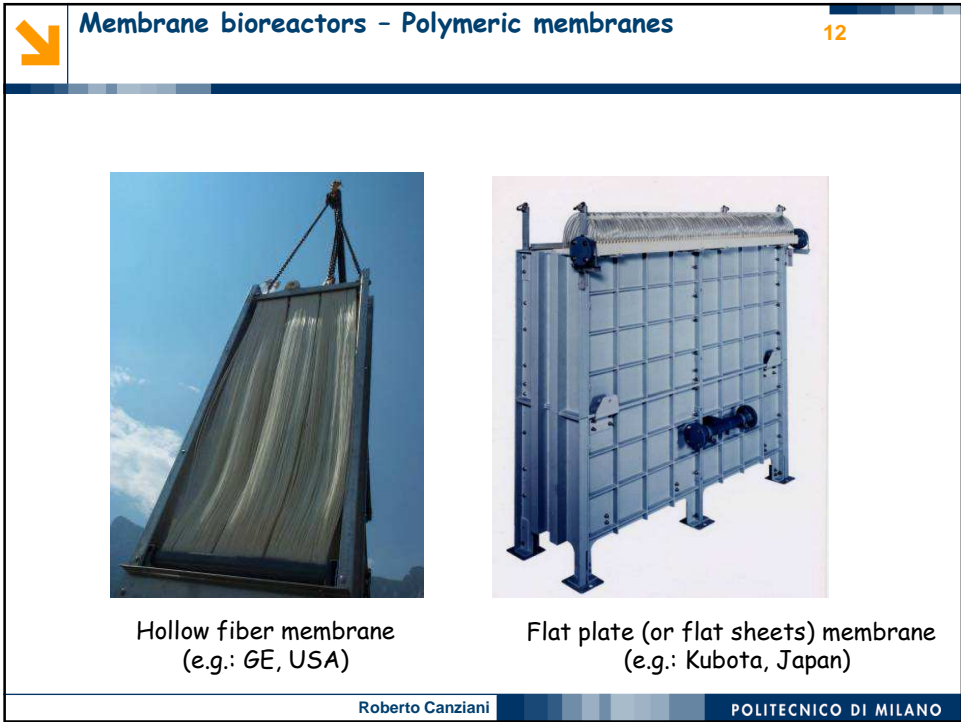
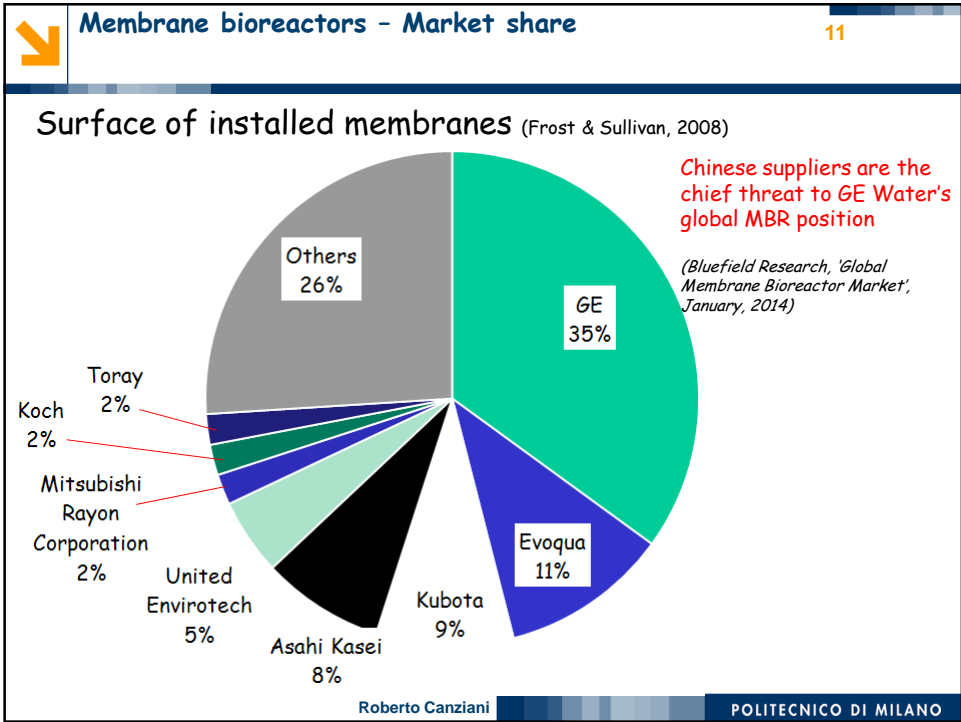
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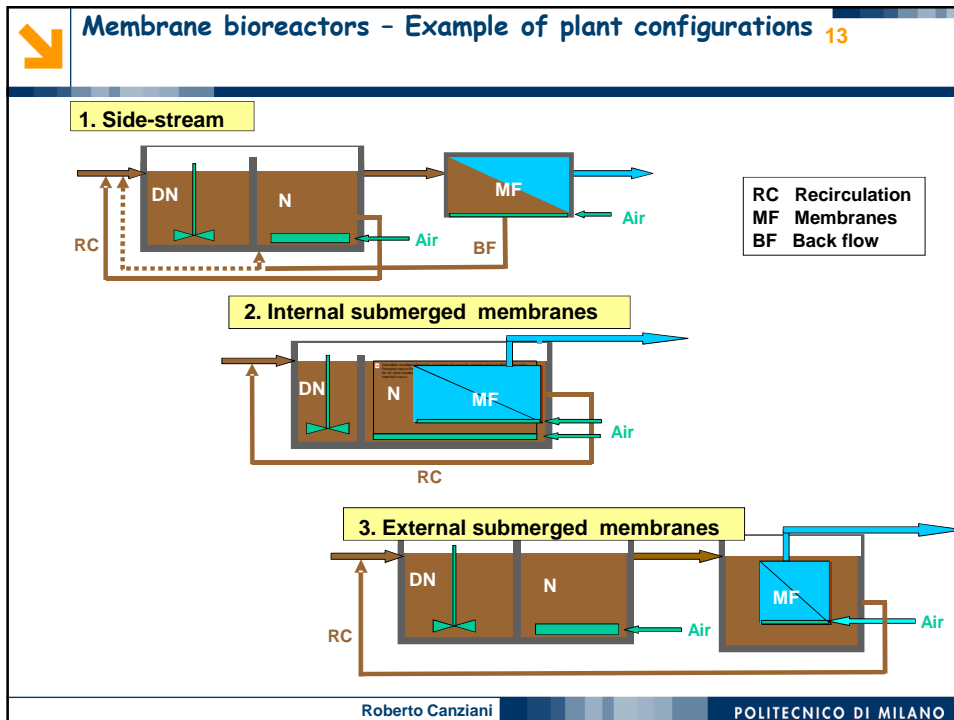
### Membrane bioreactors - Market share

CAGR: Compound Annual Growth Rate

	\$ Billion	Market Share (%)	CAGR 2010-2015		
			Low (<5%)	Med (5-8%)	High (> 8%)
<b>Membrane Bioreactors (MBR)</b>	0.7	1.9	→ Very High		
RO	1.0	5.4	→ High		
MF	1.0	2.8	→ High		
UF	1.2	3.5	→ High		
NF	0.4	1.3	→ Med		
UV	0.5	1.6	→ High		
Ozone	0.1	0.6	→ High		
UASB (Municipal)	0.2	0.5	→ High		
Chlorination	1.1	3.5	→ Med		
Deminalisation	0.8	2.4	→ Med		
WW Pre-Treatment	1.4	4.2	→ Low		
W&WW Clarifiers	3.5	9.9	→ Med		
Other Primary WW	3.8	11.1	→ Med		
Activated Sludge	3.7	10.7	→ Med		
Other Biological WW	4.0	10.9	→ Med		
Sludge Thickening	1.5	4.4	→ Low		
Sludge Dewatering	1.8	5.2	→ High		
Sludge Digestion	0.7	2.0	→ High		
Sludge Drying	0.7	2.0	→ High		
Filtration	5.5	16.0	→ Med		

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### Membrane bioreactors vs CAS 14

**Membrane:**  
solid-liquid separation device  
*(instead of gravity settling)*

- ➔ SRT independent from HRT
- ➔ SS concentration: 3 to 4 times higher than in CAS processes
- ➔ Biomass selection

does not occur by settling ability,  
BUT  
on adaptation to process conditions  
and available substrate

In an MBR process these units are not needed

secondary settling

disinfection

filtration

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## Membrane bioreactors vs CAS

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CLAIM: MBR are better than CAS because:

- ❖ Bulking and biological foams are no longer a problem
- ❖ Stricter effluent limits can be met
- ❖ Revamping and upgrading can be done with little room available

Activated Sludge Process

Raw Water

Reaction tank

Sedimentation Tank

Disinfection Tank

Treated Water

MBR

Raw Water

Treated Water

sludge

permeate

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## Membrane bioreactors - Challenges

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- Fouling (and cleaning)
- Energy demand (mainly for aeration)
- Investment and operating costs

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Membrane bioreactors - Fouling ("Achille's heel of MBRs")<sup>17</sup>

"The process resulting in **loss of performance of a membrane** due to the **deposition of suspended or dissolved substances on its external surface, at its pores openings or within its pores**"

William J. Koros, 1996, JMS



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Membrane bioreactors - Fouling - 1<sup>18</sup>

According to Zhang *et al.* (JMS, 2006, 284, 54-66)

- 1<sup>st</sup> stage - Conditioning
  - **Fouling even @ no flux** (passive adsorption of macromolecules)
  - **Initial pore blocking**
- 2<sup>nd</sup> stage - Steady-state Fouling
  - **Cake formation**
  - **Biofilm growth**
  - **Further pore blocking** (removable by chemical and physical cleaning)
- 3<sup>rd</sup> stage (to be avoided) - **TMP jump**  
permeability collapses;  $J > \text{critical } J$  (severe irreversible fouling)

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**Membrane bioreactors - Fouling - 2** 19

The diagram illustrates the cycle of membrane fouling and cleaning. It starts with a 'New membrane' (orange blocks). 'Initial filtration' occurs, where 'Sludge flocs' (grey spheres), 'Colloids' (green circles), and 'Solutes' (black dots) begin to accumulate on the membrane surface. 'Long-term filtration' leads to 'Removable fouling and irremovable fouling', where a thick layer of sludge flocs and colloids has built up. 'Physical cleaning' (indicated by a curved arrow) removes the 'Removable fouling', leaving behind 'Irremovable fouling' (solutes and some colloids). 'Chemical cleaning' (indicated by a curved arrow) then removes the 'Irremovable fouling', returning the membrane to its 'New membrane' state.

**Legend:**  
 ● Sludge flocs  
 ● Colloids  
 ● Solutes

SOURCE: Meng, F.; Chae, S.-R.; Drews, A.; Kraume, M.; Shin, H.-S.; Yang, F. Recent advances in membrane bioreactors (MBRs): Membrane fouling and membrane material. Water Res. 2009, 43, 1489-1512.

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**Membrane bioreactors - Fouling - 3** 20

The diagram shows the mechanism of fouling. 'High Velocity Cross-Flow' is applied to the 'Membrane' surface. This creates a 'Fouling Boundary Layer' where 'Low Shear' conditions prevail, allowing particles to settle and form a fouling layer. 'Plugged Pores' are shown where particles have entered the membrane's pores. To the right, two microscopy images compare a 'Clean' membrane surface (smooth and grey) with a 'Fouled' membrane surface (covered in a thick, porous grey layer).

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**Membrane bioreactors - Fouling - 4: New developments** 21

Membrane treated to induce low-fouling properties

- Plasma treatment
- Antifouling materials
- Surface modification with nanoparticles

Liu, C.X.; Zhang, D.R.; He, Y.; Zhao, X.S.; Bai, R. Modification of membrane surface for anti-biofouling performance: Effect of anti-adhesion and anti-bacteria approaches. *J. Membr. Sci.* **2010**, *346*, 121–130  
 Petros K, Gkotsis, Dimitra Ch, Banti, Efrosini N, Peleka, Anastasios I, Zouboulis and Petros E. Samaras Fouling Issues in Membrane Bioreactors (MBRs) for Wastewater Treatment: Major Mechanisms, Prevention and Control Strategies, *Processes*, **2014**, *2*(4), 795-866; doi:10.3390/pr2040795

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**Membrane bioreactors - Fouling - 5: Flux enhancers** 22

**PACI addition for fouling control**

Resistance to filtration ( $10^{12} \text{ m}^{-1}$ )

time (days)

control period      PACI dosage period

reversible resistance (removable by physical cleaning, relaxation)

irreversible resistance (partially removable by chemical cleaning)

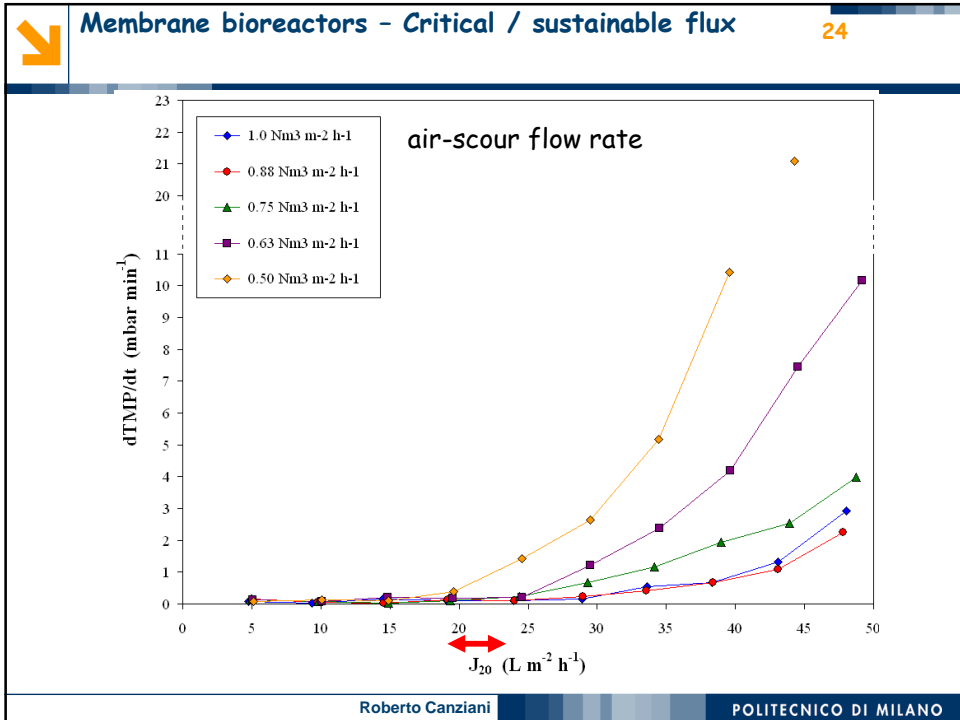
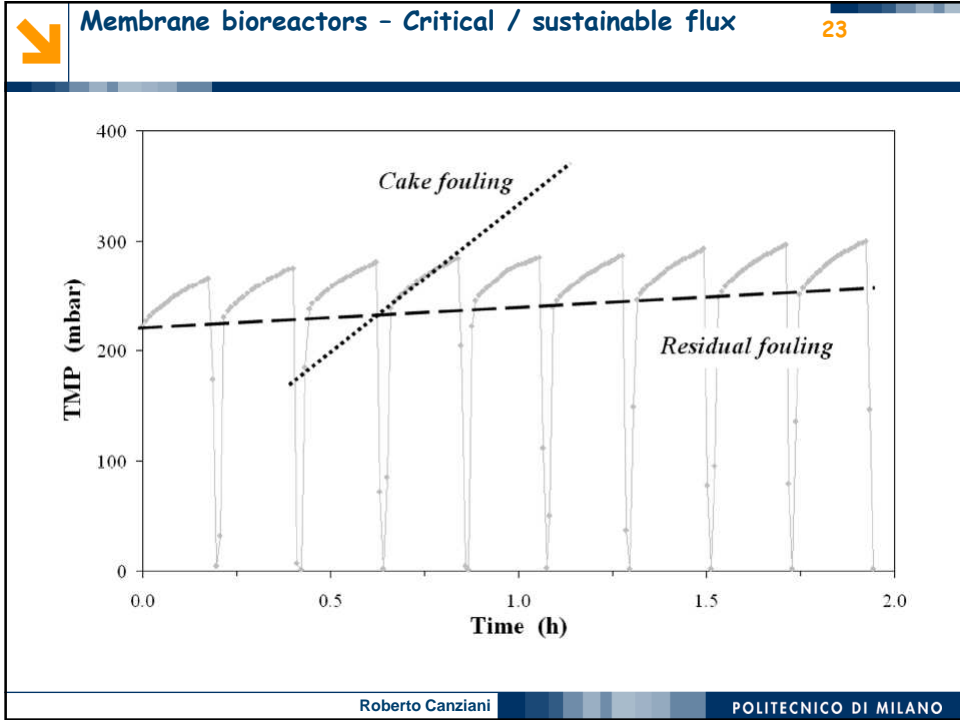
membrane resistance

- more stable filtration process
- reduction (- 45%) of the irreversible fouling rate

Other flux enhancers:

- cationic polymers
- activated carbon

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**Membrane bioreactors - Backwash** 25

**Periodical backwash**

**Normal Operations**

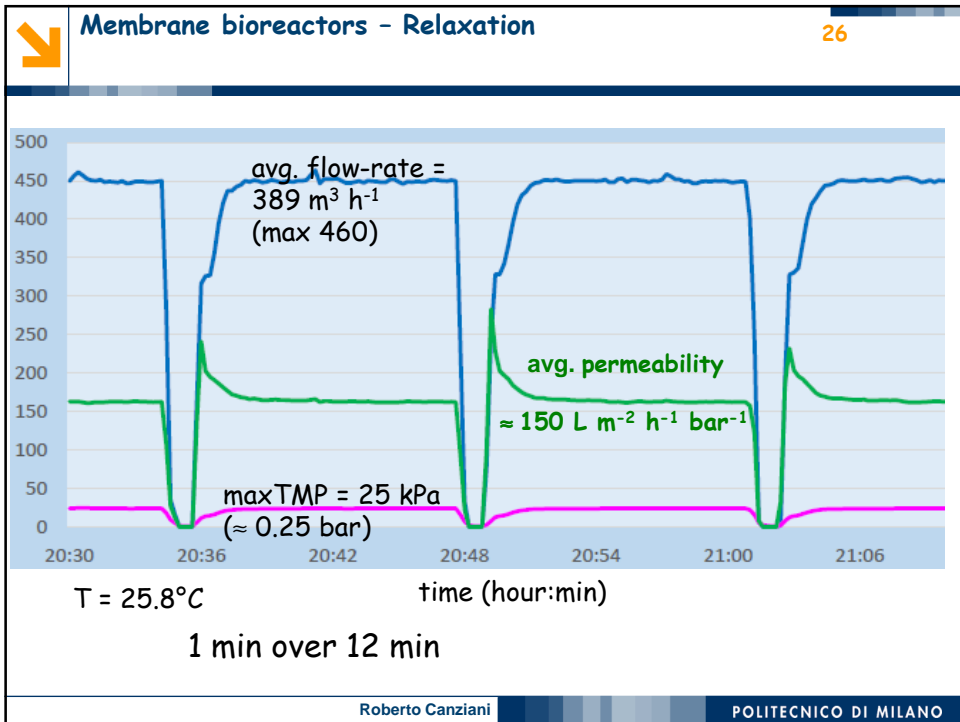
Feed Stream  
Clean filtrate  
Contaminants  
Membrane Wall

**Backwash Operations**

Permeate  
Contaminants Dislodged by permeate

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**Membrane bioreactors - Clogging** 27

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**Membrane bioreactors - Cleaning - 1** 28



Borghetto S. Spirito (Ligurian Sea, Italy)

At present the MBR modules treat 25.000 AE ( $Q_m = 280 \text{ m}^3 \text{ h}^{-1}$ )

Cleaning Service	No. per year	HClO (L)	Citric acid (L)
Planned maintenance washings	192	11.500	-
Emergency washings	4	250	-
Soak and wash	16	6.900	3.500
<b>Total</b>	<b>212</b>	<b>19.000</b>	<b>3.500</b>

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Membrane bioreactors - Cleaning - 2 29



Empty the tank    ... then soak

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Membrane bioreactors - Cleaning - 3 30

... and wash



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**Membrane bioreactors - Cleaning - 4** 31

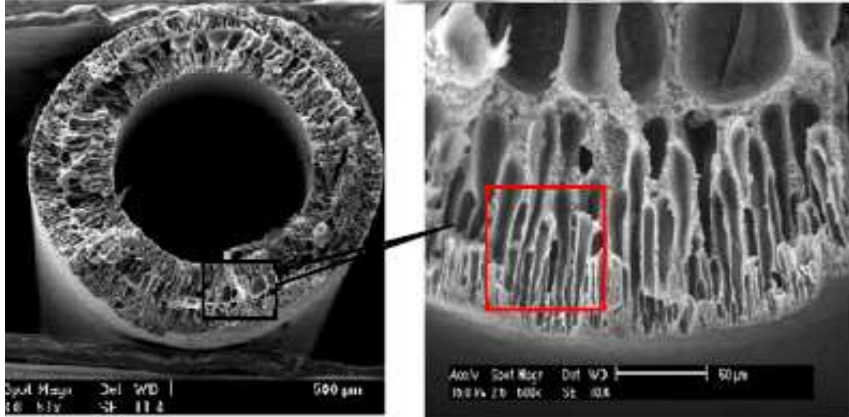
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**Membrane bioreactors - Cleaning - 5** 32

HF membrane after physical cleaning

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**Membrane bioreactors - Cleaning - 6** 33

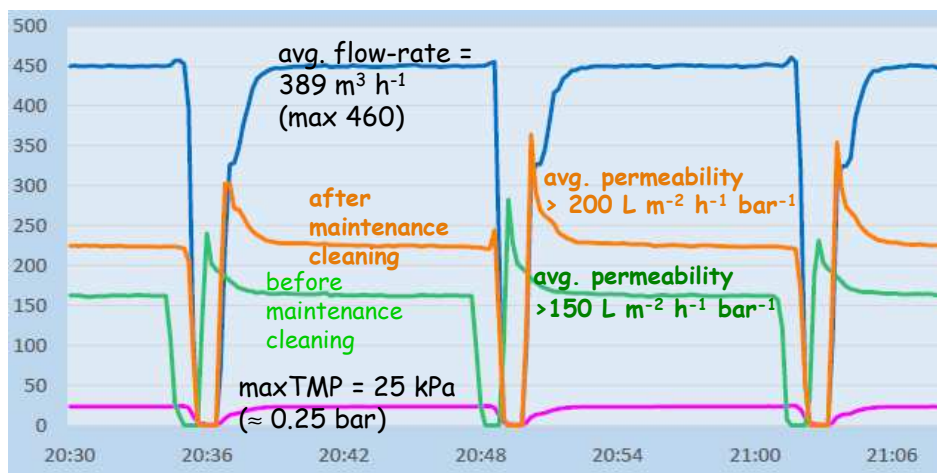


HF membrane after physical AND chemical cleaning  
Source: Li et al., 2014

The Membrane Fouling Monitored by Scanning Electron Microscopy (SEM) in a Submerged Membrane Bioreactor  
*Journal of Water Sustainability*, Volume 4, Issue 3, September 2014, 159-166

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**membrane bioreactors - Cleaning - 7** 34



avg. flow-rate =  $389 \text{ m}^3 \text{ h}^{-1}$  (max 460)

after maintenance cleaning  
avg. permeability  $> 200 \text{ L m}^{-2} \text{ h}^{-1} \text{ bar}^{-1}$

before maintenance cleaning  
avg. permeability  $> 150 \text{ L m}^{-2} \text{ h}^{-1} \text{ bar}^{-1}$

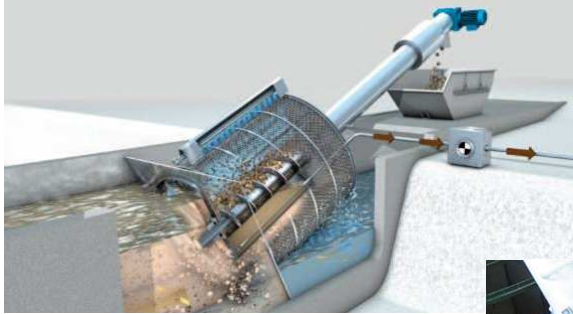

maxTMP = 25 kPa ( $\approx 0.25 \text{ bar}$ )

T = 25.8°C

time (hour:min)

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**Membrane bioreactors - Pretreatments** 35

rotating fine screens are a "must", to prevent failures (spacing: 0,75 to 2 mm)

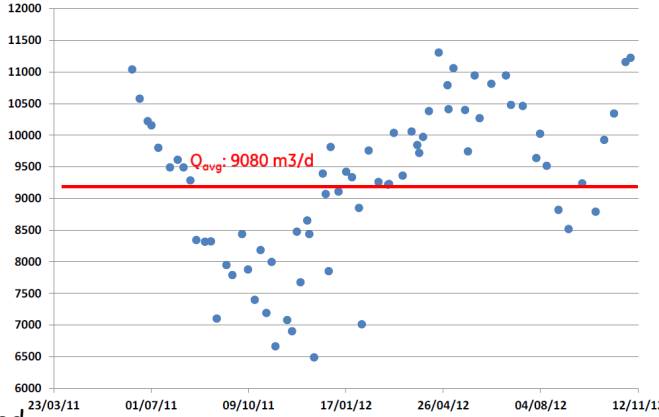
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**Membrane bioreactors - Management of variable flow rates** 36

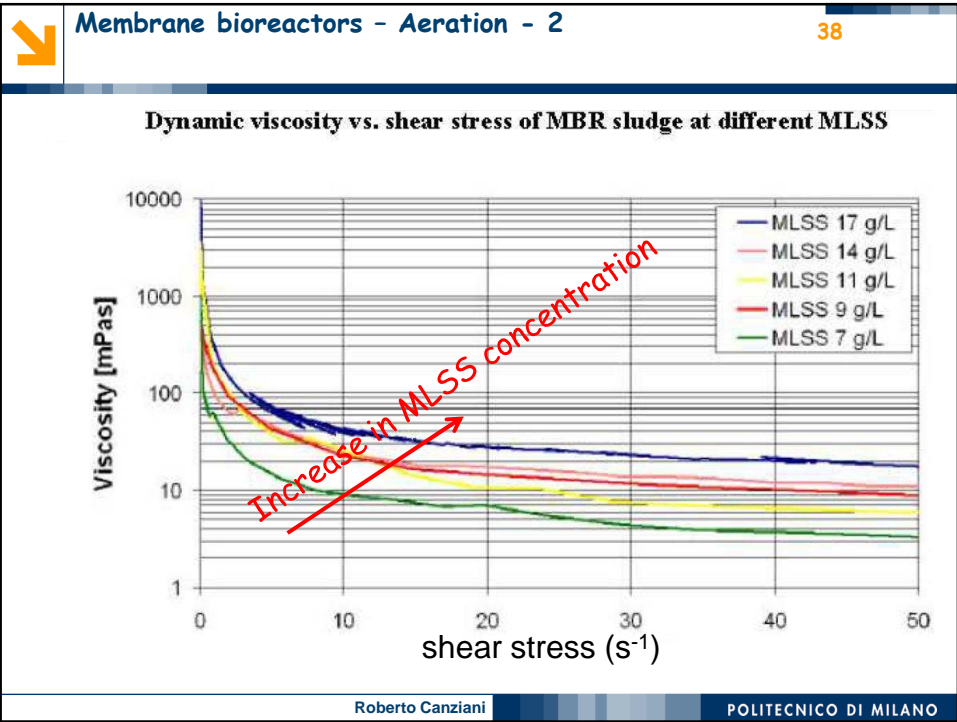
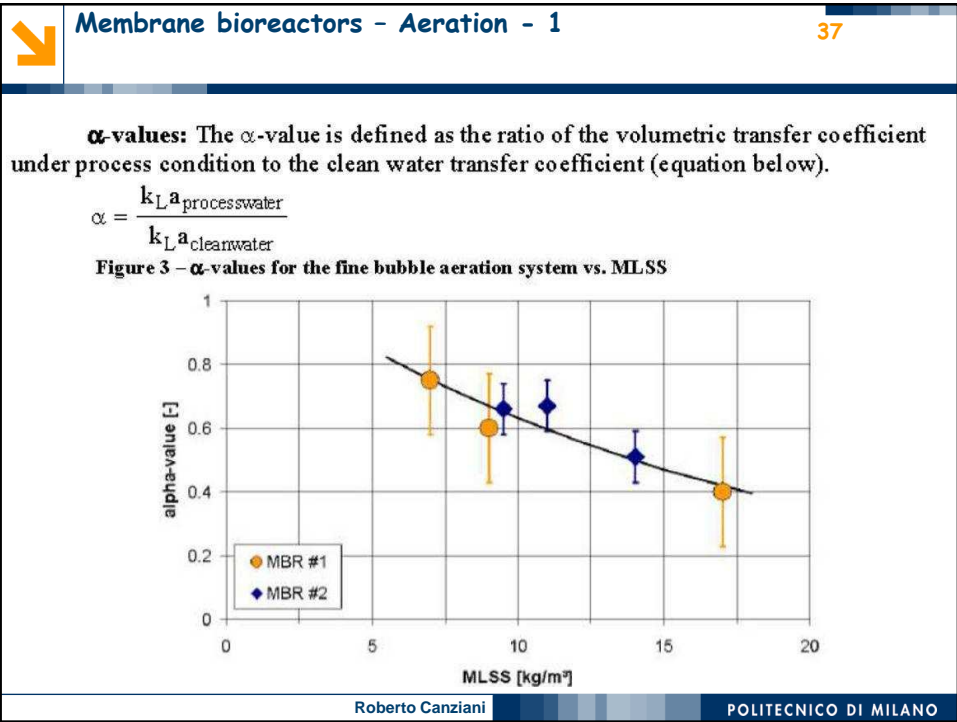
**MBR can cope with 2-fold variation**

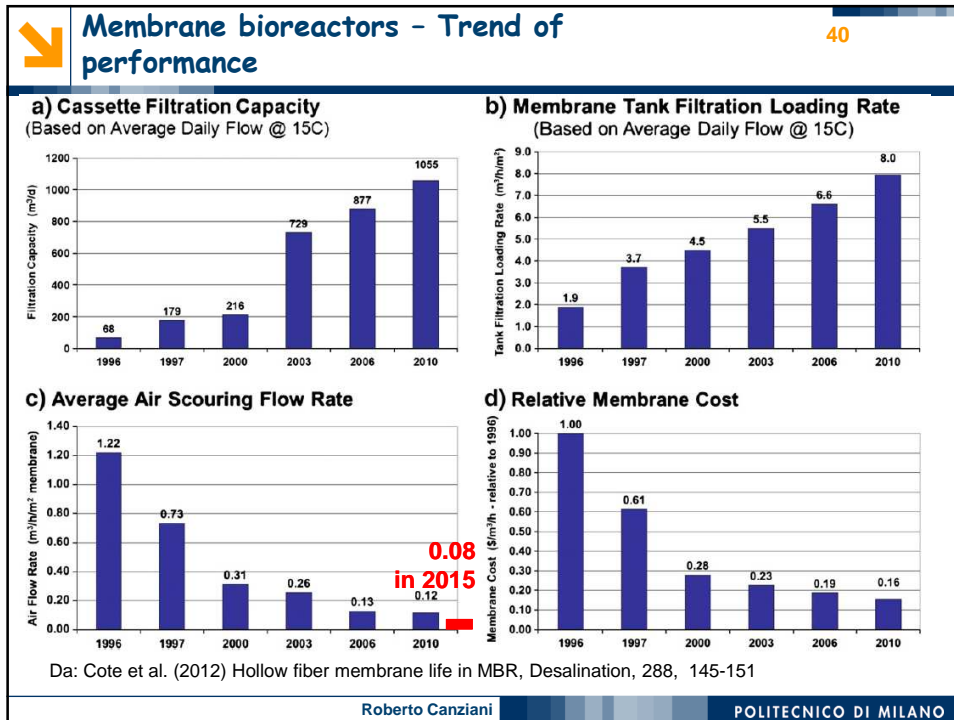
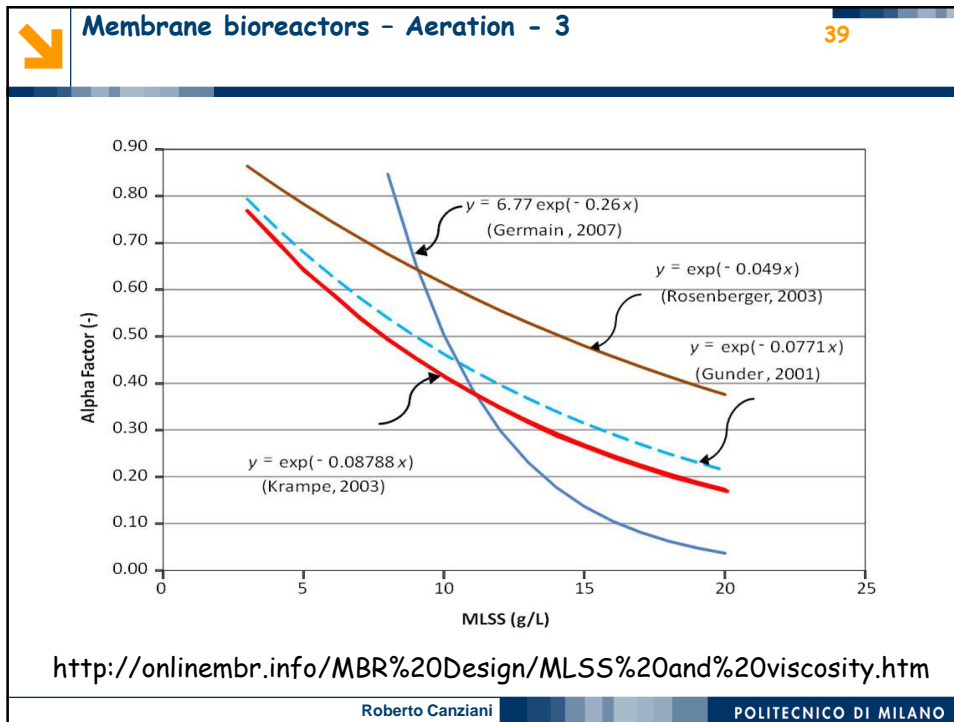
**Dry weather:** equalization tanks may be useful

**Wet weather flowrates** in combined sewer systems: side stream treatments may be required



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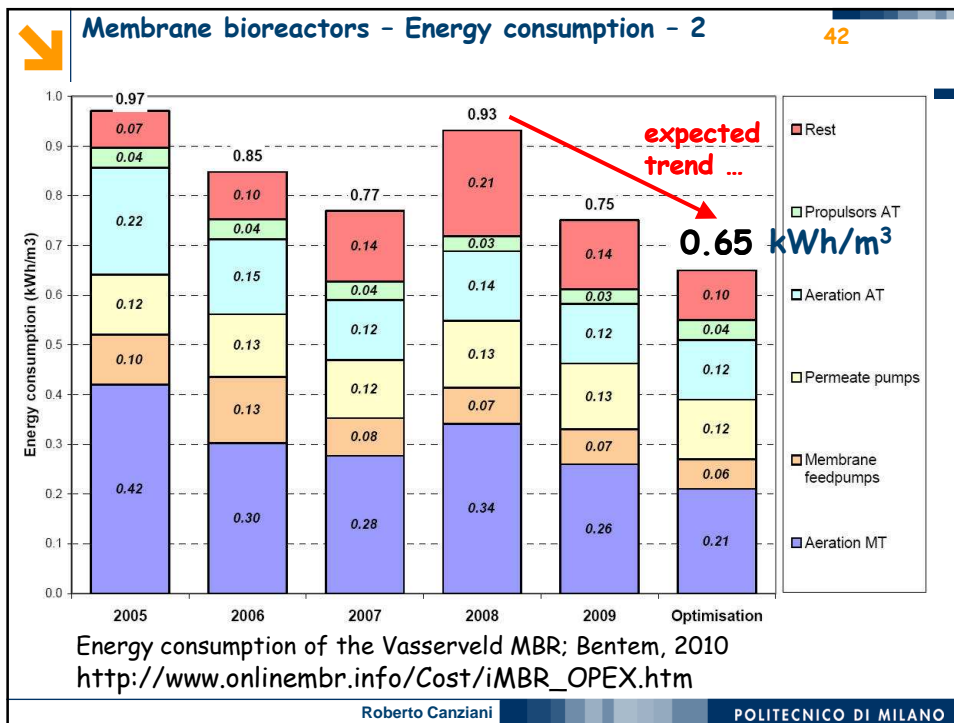


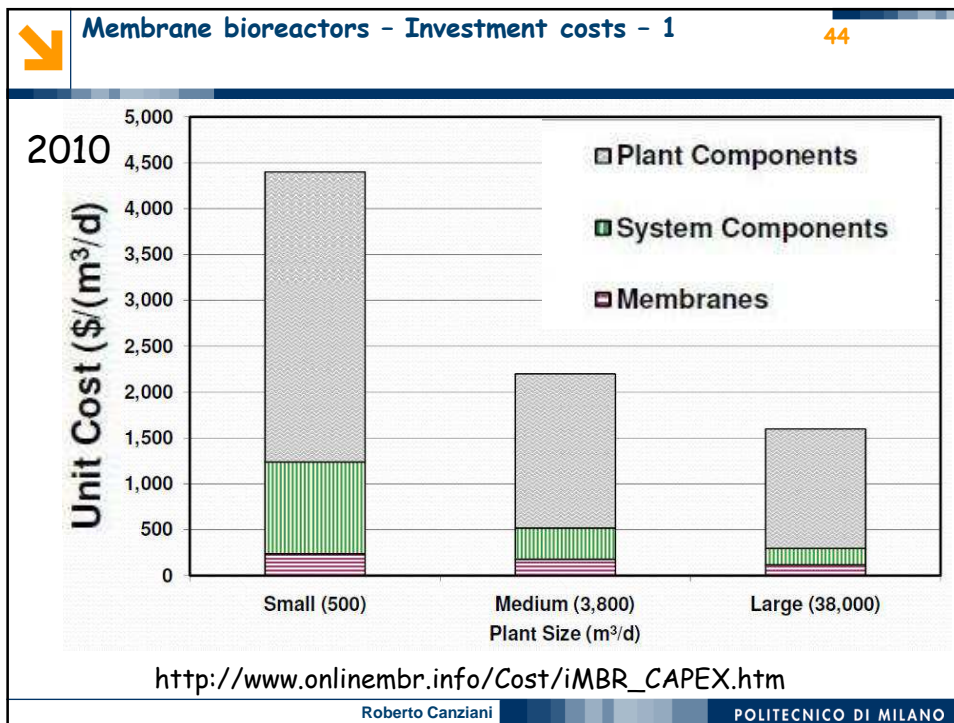
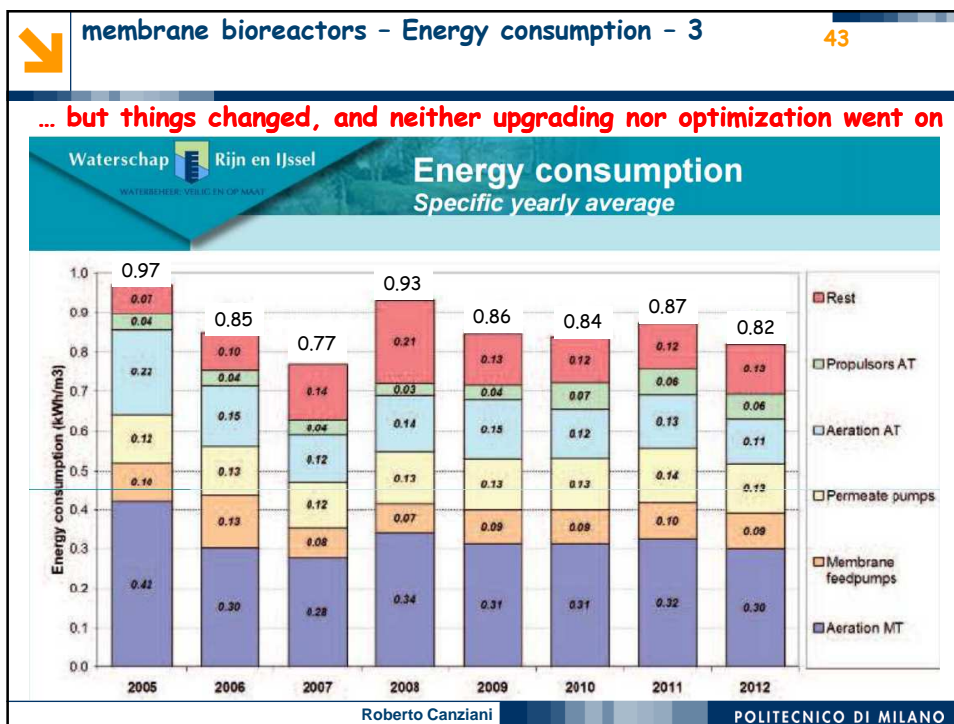
**Membrane bioreactors - Energy consumption - 1** 41

Treatment unit	Specific energy (kWh/m <sup>3</sup> )
Pre-treatments	0.03
Nitrification - denitrification	0.20
MBR units	0.23
Others (aerobic sludge stabilization, thickening and dewatering, odour control, general plant services)	0.21
<b>TOTAL</b>	<b>0.67</b>

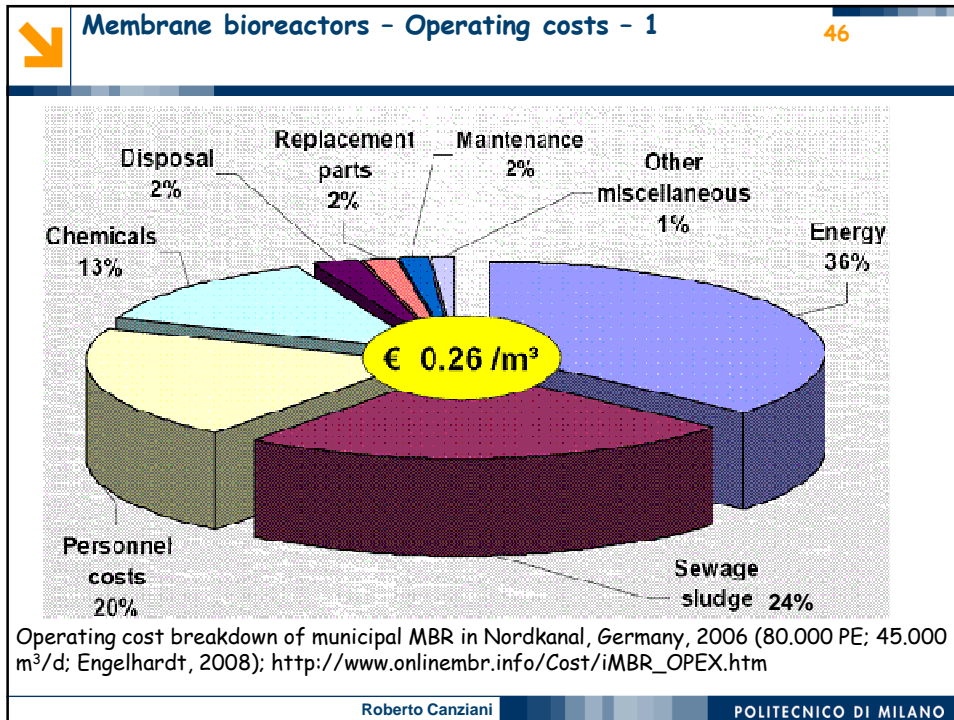
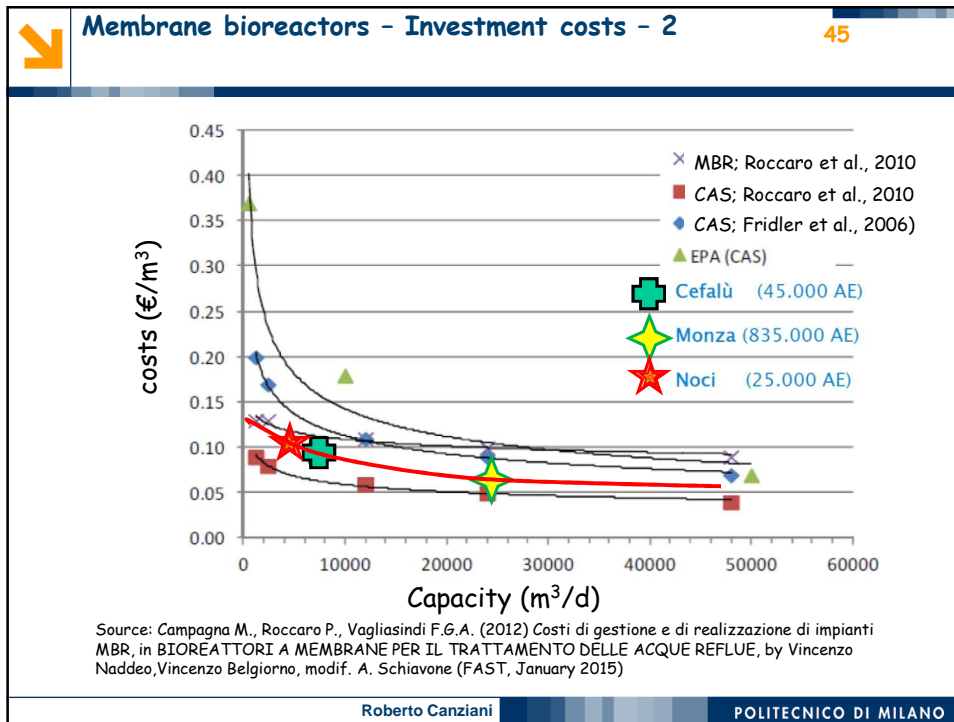
WWTP Borghetto S. Spirito, 2014

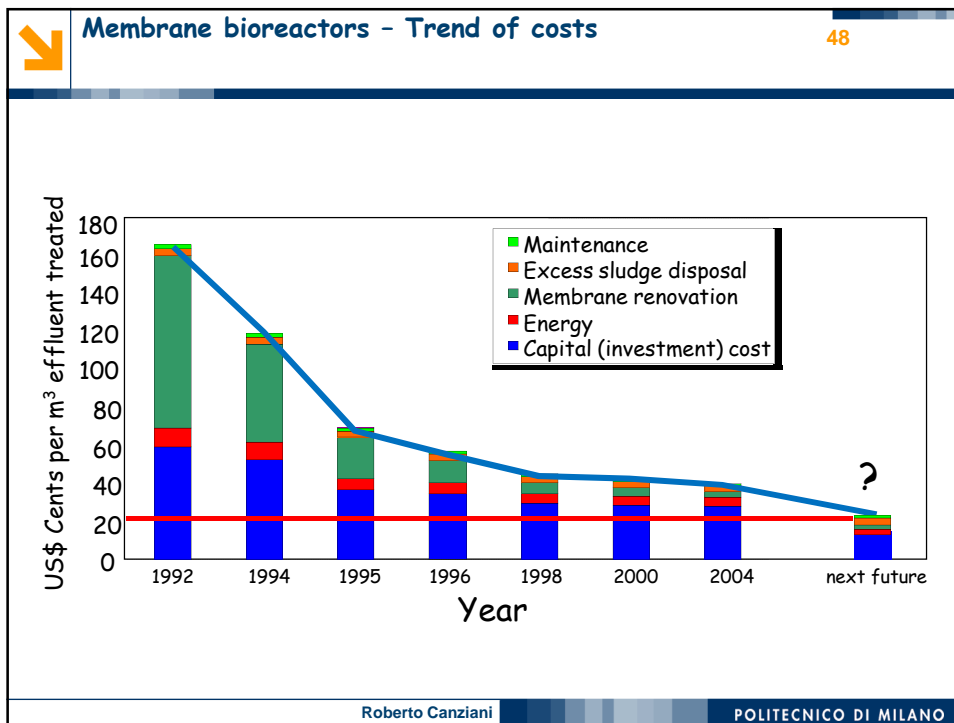
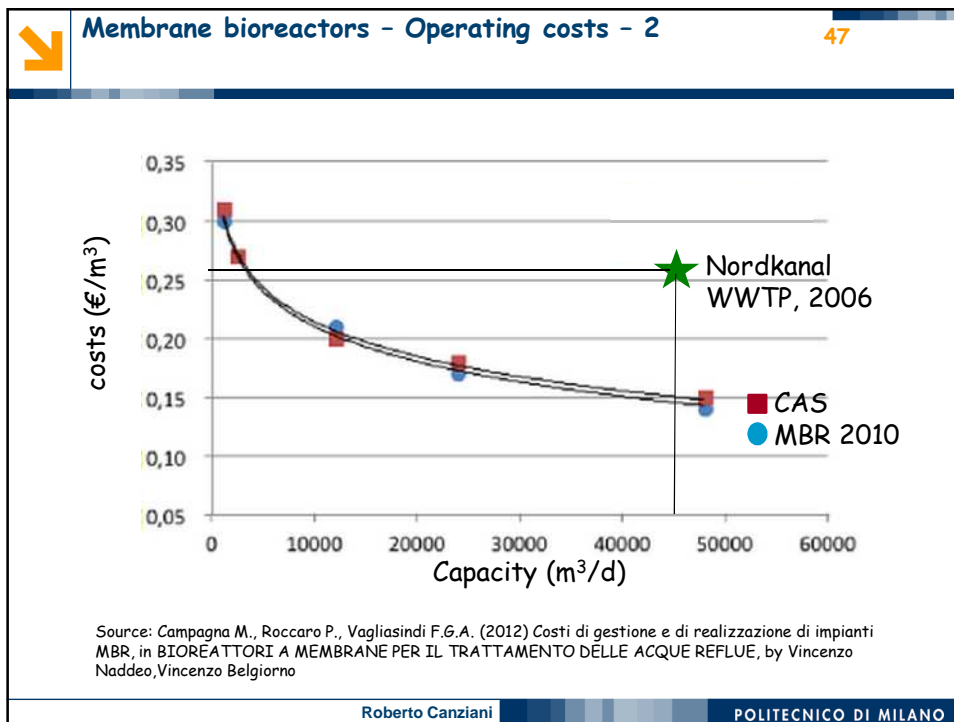
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**Membrane bioreactors - HF: Strengths and lessons learned**

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❑ Advantages of HF vs SF:

- Higher packing density → lower footprint
- High flexibility → better adaptation to local needs
- Lower energy required for air scouring
- Can sustain effective backwashing

❑ Lessons learned:

- Risk of membrane abrasion
- Ragging inside the cassette → 
- Possible delamination
- Higher risk of debris accumulation
- In some cases (high  $\Delta T$ ) slack-adjustment is necessary
- Fiber may slip-off from top header

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**Membrane bioreactors - SF: Strengths and lessons learned**

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❑ Advantages of SF vs HF:

- Lower fouling potential by debris (fibers, rags, hair)
- Lower TMP applied (or higher LMH at same TMP)
- Lower consumption of chemicals

❑ Lessons learned:

- Lower *packing-density* → *higher footprint*  
→ *internal submerged configuration may be the only design choice*
- Risk of uneven flux distribution
- Backwash may be unefficient
- De-lamination risk even at low backwashing pressure

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**Membrane bioreactors - Possible future developments - 1** 51

### Hybrid (combination of MBR and other treatments)

**Anaerobic MBRs**      **Non-woven membranes**

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**Membrane bioreactors - Possible future developments - 2** 52

To co-generation system

A small amount of high-strength organic waste (kitchen waste, disposer-wastewater and toilet flushing)

Urine separation is also worthwhile to be considered

Anaerobic pretreatment  
Methane production

A large amount of diluted organic wastewater (graywater)

Biomass production from liquid organic waste  
Aerobic MBR

Safe effluent

(\*) N,P recovery option

(A very small amount of residue)

- Renewable energy utilization
- IT-based maintenance service system
- User participation in monitoring

**Next-generation MBR system: anaerobic combination for on-site small-scale advanced treatment.**

F. I. Hai and K. Yamamoto, Membrane Biological Reactors, 2011  
<http://ro.uow.edu.au/cgi/viewcontent.cgi?article=2198&context=scipapers>

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Membrane bioreactors 53

# Thank you for your attention

## Acknowledgements

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<http://hidroinformatics.polimi.it>

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Membrane bioreactors - TMP and Flux 54

Permeability:  
 $K = J/TMP$

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